

Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for $C_mH_{2m+1}(OCH_2CH_2)_nOH$ ($m = 1$ or 2 or 4 and $n = 1$) + Benzene, + Toluene, + (*o*-, *m*-, and *p*-) Xylenes, + Ethylbenzene, and + Cyclohexane

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Measurements on densities, speeds of sound, viscosities, and relative permittivities for 21 binary mixtures of alkoxyethanols (2-methoxyethanol, 2-ethoxyethanol, and 2-butoxyethanol) + benzene, + toluene, + (*o*-, *m*-, and *p*-) xylenes, + ethylbenzene, and + cyclohexane at different temperatures are reported. The excess molar volumes, excess isentropic compressibilities, deviations in dynamic viscosities, speeds of sound, and relative permittivities have been calculated across the mole compositions. The compositional variation of excess and deviation functions has been expressed in terms of the Redlich–Kister equation.

Introduction

The molecules with the general formula $C_mH_{2m+1}(OCH_2CH_2)_nOH$ display a wide range of interesting properties and association patterns both in van der Waals clusters^{1,2} and in the condensed phase.^{3–7} These characteristics result from interplay of (i) the relative importance of the polar and nonpolar fragments, (ii) conformational degrees of freedom, (iii) the occurrence of intramolecular hydrogen bonding type interactions, and (iv) the extent of intermolecular interactions, hydrogen bonding included. The molecules with $m = 1, 2,$ and 4 and $n = 1$ are widely used industrial solvents. Besides, these molecules act as model compounds for understanding the structural dynamics of poly(oxyethylene) crown ethers and related compounds.⁸ There are several reports in the literature on the measurements of excess molar enthalpies, H_m^E ,^{9,10} excess molar volumes, V_m^E ,^{9–12} excess isentropic compressibilities, κ_s^E ,^{9–12} excess viscosities, η^E ,¹³ and vapor–liquid equilibria^{9,10} for the lower alkoxyethanols + *n*-aliphatic alkanes. It is generally concluded that *n*-alkanes disrupt the self-associated structures of alkoxyethanols and such disruptions become more with the increase in the chain length of *n*-alkanes. Few available studies^{14–16} on the thermodynamic behavior of alkoxyethanols + aromatic hydrocarbons in terms of calculated V_m^E and H_m^E suggested that aromatic hydrocarbons can form weak complexes with the former. With a view to understand the binary systems of alkoxyethanols + aromatic hydrocarbons further, the present study reports various excess and deviation functions, namely, V_m^E , viscosity deviations, $\delta\eta$, deviations in speeds of sound, δv , κ_s^E , and deviations in relative permittivities, $\delta\epsilon_r$, as calculated from the measured densities, ρ , dynamic viscosities, η , speed of sound, v , and relative permittivities, ϵ_r , for 2-methoxyethanol, 2-ethoxyethanol, or 2-butoxyethanol + aromatic hydrocarbons (benzene, toluene, *o*-, *m*-, *p*-xylenes, ethylbenzene) or + cyclohexane mixtures at different temperatures.

Experimental Section

Materials. 2-Methoxyethanol, 2-ethoxyethanol, and 2-butoxyethanol were Chiti-Chem, India, products with a stated purity of 99.5% on a mole basis. These chemicals were dried over 4 Å molecular sieves and three times fractionally distilled through a 15 plate column under vacuum with temperature maintained at 100 °C. This procedure reduced the various initial impurities such as water, free acid (as CH_3COOH), and carbonyl compounds. A reagent grade benzene was acquired locally and purified by a standard procedure.¹⁷ Toluene and *o*-, *m*-, and *p*-xylenes obtained from Chiti-Chem, India, were further purified by successive shaking with concentrated sulfuric acid, sodium hydroxide solutions, and mercury. They were dried over phosphorus pentoxide and then finally fractionally distilled over a 1 m column. Ethylbenzene procured from Chiti-Chem, India, was of analytical reagent (AR) quality with 99.5% purity (on a mole basis). It was further purified by shaking with concentrated sulfuric acid until the acid layer became colorless and then with sodium carbonate solution and water. Afterward, it was dried over anhydrous magnesium sulfate and fractionally distilled. Cyclohexane was of AR grade from Chiti-Chem, India. It was washed several times in the cold with a mixture of concentrated nitric and sulfuric acids to nitrate any benzene that may have been present. After repeated washings with distilled water, it was fractionally distilled over sodium metal.

Methods. The binary solutions were prepared by mass in hermetically sealed glass vials. The solutions of each composition were prepared fresh, and all the properties were measured the same day. The mass measurements, accurate to ± 0.01 mg, were made on a single pan analytical balance (Dhona 100 DS, India). The estimated accuracy in the mole fraction was ± 0.0001 .

Densities of the pure liquids and their mixtures were measured with a high precision vibrating tube digital density meter (Anton Paar, DMA 5000). The instrument has a built-in thermostat for maintaining desired temperatures in the range 0 to 90 °C. The repeatability of the

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Table 2. (Continued)

x_1	$\rho/\text{g}\cdot\text{cm}^{-3}$				x_1	$\rho/\text{g}\cdot\text{cm}^{-3}$			
	$T=298.15\text{ K}$	$T=303.15\text{ K}$	$T=308.15\text{ K}$	$T=313.15\text{ K}$		$T=298.15\text{ K}$	$T=303.15\text{ K}$	$T=308.15\text{ K}$	$T=313.15\text{ K}$
2-Ethoxyethanol (1) + Ethylbenzene (2)					2-Ethoxyethanol (1) + Cyclohexane (2)				
0.0573	0.864 51(6)	0.860 19(2)	0.855 98(5)	0.851 18(3)	0.0542	0.779 45(6)	0.773 87(7)	0.769 63(2)	0.764 48(3)
0.1487	0.868 36(6)	0.863 91(3)	0.859 68(4)	0.854 70(5)	0.1507	0.790 32(8)	0.784 68(7)	0.780 34(1)	0.775 04(0)
0.2498	0.873 45(9)	0.868 92(6)	0.864 73(3)	0.859 54(4)	0.2541	0.803 24(7)	0.797 74(6)	0.793 57(0)	0.788 10(9)
0.3527	0.879 37(9)	0.874 82(7)	0.870 72(4)	0.865 32(0)	0.3508	0.816 47(9)	0.811 19(4)	0.807 22(2)	0.801 61(6)
0.4489	0.885 44(6)	0.880 92(8)	0.876 94(6)	0.871 34(9)	0.4520	0.831 44(6)	0.826 39(3)	0.822 52(5)	0.816 77(3)
0.4998	0.888 82(2)	0.884 34(0)	0.880 43(2)	0.874 73(9)	0.5000	0.838 91(6)	0.833 95(8)	0.830 07(5)	0.824 25(7)
0.5485	0.892 14(2)	0.887 70(3)	0.883 87(0)	0.878 09(1)	0.5497	0.846 88(1)	0.842 00(6)	0.838 06(1)	0.832 17(7)
0.6501	0.899 29(3)	0.894 96(5)	0.891 29(6)	0.885 35(6)	0.6534	0.864 16(4)	0.859 41(4)	0.855 21(9)	0.849 20(3)
0.7484	0.906 42(4)	0.902 21(6)	0.898 70(5)	0.892 62(9)	0.7527	0.881 37(9)	0.876 70(9)	0.872 24(4)	0.866 11(2)
0.8508	0.913 99(8)	0.909 90(2)	0.906 53(8)	0.900 34(1)	0.8492	0.898 48(2)	0.893 92(3)	0.889 41(5)	0.883 18(0)
0.9547	0.921 78(2)	0.917 75(4)	0.914 50(8)	0.908 19(1)	0.9552	0.917 32(9)	0.913 07(1)	0.909 21(1)	0.902 87(7)
2-Butoxyethanol (1) + Benzene (2)					2-Butoxyethanol (1) + Toluene (2)				
0.0553	0.874 30(5)	0.869 03(8)	0.863 89(8)	0.858 82(1)	0.0550	0.863 84(6)	0.859 17(3)	0.854 65(1)	0.849 76(8)
0.1496	0.876 28(2)	0.871 10(7)	0.866 19(2)	0.860 98(6)	0.1509	0.867 24(8)	0.862 55(5)	0.858 08(1)	0.852 99(5)
0.2488	0.879 00(8)	0.873 93(1)	0.869 18(5)	0.863 87(4)	0.2513	0.871 21(9)	0.866 52(5)	0.861 96(0)	0.856 75(6)
0.3504	0.882 07(4)	0.877 10(4)	0.872 51(4)	0.867 12(7)	0.3489	0.875 19(9)	0.870 52(3)	0.865 88(4)	0.860 60(5)
0.4555	0.885 22(0)	0.880 36(6)	0.875 95(6)	0.870 52(2)	0.4511	0.879 27(0)	0.874 63(4)	0.870 03(4)	0.864 68(1)
0.4995	0.886 47(3)	0.881 67(0)	0.877 34(6)	0.871 90(1)	0.5015	0.881 19(2)	0.876 58(3)	0.872 06(1)	0.866 66(8)
0.5504	0.887 85(4)	0.883 11(0)	0.878 89(6)	0.873 44(1)	0.5525	0.883 06(2)	0.878 48(5)	0.874 08(2)	0.868 64(6)
0.6482	0.890 26(2)	0.885 63(5)	0.881 65(5)	0.876 19(3)	0.6512	0.886 44(1)	0.881 93(6)	0.877 86(3)	0.872 33(7)
0.7535	0.892 46(2)	0.887 96(2)	0.884 26(1)	0.878 79(7)	0.7494	0.889 48(6)	0.885 06(1)	0.881 39(1)	0.875 78(7)
0.8483	0.894 11(1)	0.889 72(2)	0.886 27(2)	0.880 80(4)	0.8498	0.892 31(7)	0.887 97(8)	0.884 68(9)	0.879 04(7)
0.9556	0.895 67(0)	0.891 40(1)	0.888 20(2)	0.882 71(1)	0.9541	0.895 06(2)	0.890 80(7)	0.887 71(9)	0.882 13(6)
2-Butoxyethanol (1) + <i>o</i> -Xylene (2)					2-Butoxyethanol (1) + <i>m</i> -Xylene (2)				
0.0549	0.875 83(5)	0.871 65(1)	0.867 29(9)	0.862 92(4)	0.0560	0.861 44(5)	0.857 06(3)	0.852 68(1)	0.847 76(8)
0.1475	0.876 80(6)	0.872 55(7)	0.868 23(9)	0.863 54(7)	0.1520	0.864 52(2)	0.859 92(4)	0.855 46(7)	0.850 37(8)
0.2508	0.878 94(6)	0.874 52(2)	0.870 30(8)	0.865 35(1)	0.2496	0.868 18(9)	0.863 47(2)	0.859 11(0)	0.853 77(2)
0.3485	0.881 54(2)	0.876 95(1)	0.872 86(4)	0.867 70(6)	0.3506	0.872 30(4)	0.867 54(8)	0.863 37(7)	0.857 79(7)
0.4527	0.884 51(1)	0.879 80(9)	0.875 86(1)	0.870 54(1)	0.4512	0.876 51(3)	0.871 78(5)	0.867 82(9)	0.862 08(3)
0.5000	0.885 84(0)	0.881 12(1)	0.877 23(4)	0.871 85(8)	0.5022	0.878 63(4)	0.873 93(8)	0.870 08(6)	0.864 29(7)
0.5489	0.887 16(9)	0.882 45(8)	0.878 63(0)	0.873 20(6)	0.5529	0.880 70(9)	0.876 05(5)	0.872 29(8)	0.866 49(3)
0.6483	0.889 66(1)	0.885 03(7)	0.881 32(5)	0.875 83(4)	0.6487	0.884 49(2)	0.879 93(4)	0.876 32(7)	0.870 56(6)
0.7518	0.891 90(6)	0.887 44(7)	0.883 85(6)	0.878 33(3)	0.7505	0.888 25(5)	0.883 81(0)	0.880 32(6)	0.874 68(4)
0.8493	0.893 72(0)	0.889 42(6)	0.885 97(4)	0.880 44(6)	0.8511	0.891 68(0)	0.887 34(2)	0.883 96(8)	0.878 45(6)
0.9524	0.895 45(2)	0.891 25(0)	0.888 00(5)	0.882 48(8)	0.9549	0.894 92(0)	0.890 67(0)	0.887 45(3)	0.881 98(6)
2-Butoxyethanol (1) + <i>p</i> -Xylene (2)					2-Butoxyethanol (1) + Ethylbenzene (2)				
0.0541	0.858 20(8)	0.853 81(6)	0.849 44(4)	0.845 15(1)	0.0546	0.863 76(5)	0.859 41(8)	0.855 27(3)	0.850 44(5)
0.1518	0.861 90(7)	0.857 46(7)	0.853 12(2)	0.848 55(1)	0.1505	0.866 73(9)	0.862 26(0)	0.858 07(9)	0.853 05(0)
0.2496	0.865 97(9)	0.861 49(6)	0.857 21(4)	0.852 27(0)	0.2513	0.870 23(5)	0.865 73(1)	0.861 49(5)	0.856 31(9)
0.3502	0.870 43(0)	0.865 91(9)	0.861 73(0)	0.856 40(4)	0.3501	0.873 92(7)	0.869 44(7)	0.865 19(8)	0.859 92(7)
0.4510	0.874 96(0)	0.870 44(7)	0.866 37(5)	0.860 74(4)	0.4528	0.877 85(6)	0.873 40(9)	0.869 23(1)	0.863 90(5)
0.5028	0.877 26(3)	0.872 76(1)	0.868 75(7)	0.863 01(5)	0.4982	0.879 58(3)	0.875 14(7)	0.871 03(1)	0.865 69(2)
0.5533	0.879 47(1)	0.874 98(6)	0.871 05(3)	0.865 23(7)	0.5500	0.881 52(6)	0.877 09(8)	0.873 07(6)	0.867 72(8)
0.6489	0.883 50(6)	0.879 07(1)	0.875 28(5)	0.869 42(1)	0.6497	0.885 14(7)	0.880 72(0)	0.876 93(6)	0.871 58(3)
0.7493	0.887 49(0)	0.883 12(5)	0.879 50(7)	0.873 71(0)	0.7511	0.888 62(3)	0.884 19(1)	0.880 68(8)	0.875 33(1)
0.8519	0.891 26(9)	0.886 97(8)	0.883 55(0)	0.877 89(2)	0.8507	0.891 81(5)	0.887 40(6)	0.884 15(4)	0.878 77(2)
0.9561	0.894 82(2)	0.890 58(8)	0.887 37(4)	0.881 84(4)	0.9614	0.895 13(4)	0.890 83(6)	0.887 73(0)	0.882 26(8)
2-Butoxyethanol (1) + Cyclohexane (2)									
0.0557	0.780 53(0)	0.774 84(4)	0.771 17(8)	0.765 44(0)					
0.1501	0.792 14(6)	0.786 38(5)	0.782 85(7)	0.776 71(4)					
0.2504	0.804 78(0)	0.799 25(3)	0.795 54(6)	0.789 54(2)					
0.3543	0.818 03(1)	0.812 87(3)	0.808 84(8)	0.803 16(7)					
0.4488	0.830 10(3)	0.825 26(1)	0.820 97(5)	0.815 49(1)					
0.5025	0.836 93(2)	0.832 23(1)	0.827 84(6)	0.822 38(1)					
0.5493	0.842 84(7)	0.838 24(1)	0.833 80(8)	0.828 29(8)					
0.6485	0.855 22(8)	0.850 72(5)	0.846 33(5)	0.840 55(8)					
0.7494	0.867 52(4)	0.863 02(4)	0.858 87(2)	0.852 71(5)					
0.8511	0.879 52(7)	0.875 01(9)	0.871 26(1)	0.864 88(1)					
0.9556	0.891 37(8)	0.887 00(3)	0.883 70(9)	0.877 70(9)					

temperature has been found to be ± 0.003 and ± 0.002 °C for a given session and two different sessions, respectively. The accuracy in the temperature during the measurements, however, is ± 0.01 °C because Pt 100 measuring sensors were used. The instrument was calibrated with air and with four times distilled and freshly degassed water at $T = (293.15, 313.15, \text{ and } 333.15)$ K during every session. The repeatabilities in the densities for the distilled water and freshly distilled pure liquids and prepared binary mixtures have been found to be better than 3×10^{-6} g·cm⁻³. We have estimated the accuracy in densities of the seven pure

liquids used in the study by comparing our data at different temperatures with the literature values, as listed in Table 1. This comparison gave a mean absolute deviation of 2.9×10^{-5} g·cm⁻³. Hence, the precision and accuracies of the densities reported in the present work are 3×10^{-6} and 2.9×10^{-5} g·cm⁻³, respectively. The viscosities, η , of pure liquids and liquid mixtures were determined using a Ubbelohde suspended-level viscometer. The viscometer was suspended in a thermostated water bath maintained to ± 0.01 °C. Four sets of readings for the flow times were taken using a Racor stopwatch that can register time to

Table 3. Parameters of Eq 2 for the Mathematical Representation of $V_m^E/\text{cm}^3 \cdot \text{mol}^{-1}$ for Alkoxyethanols (1) + Aromatic Hydrocarbons (2) and + Cyclohexane (2) at $T = (298.15 \text{ to } 313.15) \text{ K}$

T/K	a_0	a_1	a_2	$\sigma/\text{cm}^3 \cdot \text{mol}^{-1}$	a_0	a_1	a_2	$\sigma/\text{cm}^3 \cdot \text{mol}^{-1}$	a_0	a_1	a_2	$\sigma/\text{cm}^3 \cdot \text{mol}^{-1}$
	Methoxyethanol (1) + Benzene (2)				Methoxyethanol (1) + Toluene (2)				Methoxyethanol (1) + <i>o</i> -Xylene (2)			
298.15	0.548	-1.083	-0.187	0.001	0.608	-0.526	0.041	0.001	1.333	-1.192	0.406	0.001
303.15	0.697	-0.829	0.381	0.001	0.738	-0.621	0.191	0.001	1.511	-1.401	1.000	0.001
308.15	0.809	-0.970	0.439	0.001	0.844	-0.719	0.223	0.001	1.771	-1.326	0.857	0.001
313.15	0.994	-0.837	0.526	0.001	1.079	-0.525	0.184	0.001	2.034	-1.049	1.097	0.001
	Methoxyethanol (1) + <i>m</i> -Xylene (2)				Methoxyethanol (1) + <i>p</i> -Xylene (2)				Methoxyethanol (1) + Ethylbenzene (2)			
298.15	1.098	-1.178	0.861	0.001	0.899	-1.269	0.201	0.001	1.007	-1.024	0.797	0.001
303.15	1.252	-1.483	1.090	0.001	0.982	-1.301	0.190	0.001	1.125	-1.232	0.914	0.001
308.15	1.424	-1.618	1.453	0.001	1.199	-1.193	0.264	0.001	1.328	-1.363	1.067	0.001
313.15	1.692	-1.541	1.362	0.001	1.349	-1.221	0.251	0.001	1.533	-1.302	0.946	0.001
	Methoxyethanol (1) + Cyclohexane (2)				Ethoxyethanol (1) + Benzene (2)				Ethoxyethanol (1) + Toluene (2)			
298.15	3.576	0.902	2.249	0.001	0.504	-1.573	0.454	0.001	0.289	-1.082	0.766	0.001
303.15	3.798	0.912	2.027	0.001	-0.030	-1.423	0.706	0.001	0.440	-1.417	0.462	0.001
308.15	4.060	0.715	2.517	0.001	-0.280	-1.347	0.697	0.001	0.538	-1.559	0.492	0.001
313.15	4.213	0.461	3.318	0.001	-0.542	-1.272	0.681	0.001	0.603	-1.751	0.549	0.001
	Ethoxyethanol (1) + <i>o</i> -Xylene (2)				Ethoxyethanol (1) + <i>m</i> -Xylene (2)				Ethoxyethanol (1) + <i>p</i> -Xylene (2)			
298.15	0.997	-2.001	0.390	0.001	0.596	-1.677	0.468	0.001	0.525	-1.765	-0.295	0.001
303.15	1.287	-1.836	0.936	0.001	0.968	-1.964	0.650	0.001	0.677	-1.650	-0.242	0.001
308.15	1.433	-1.706	1.022	0.001	1.172	-1.838	1.336	0.001	0.713	-1.718	0.131	0.001
313.15	1.519	-1.810	1.091	0.001	1.411	-1.802	1.298	0.001	0.788	-1.783	0.368	0.001
	Ethoxyethanol (1) + Ethylbenzene (2)				Ethoxyethanol (1) + Cyclohexane (2)				Butoxyethanol (1) + Benzene (2)			
298.15	0.683	-1.470	0.424	0.001	3.170	-2.211	-0.379	0.001	0.305	-1.463	0.778	0.001
303.15	0.862	-1.667	0.394	0.001	3.255	-2.371	0.167	0.001	0.373	-1.495	0.768	0.001
308.15	0.946	-1.839	0.405	0.001	3.388	-2.029	1.466	0.001	0.527	-1.458	0.596	0.001
313.15	1.096	-1.836	0.354	0.001	3.511	-2.051	1.483	0.001	0.611	-1.533	0.576	0.001
	Butoxyethanol (1) + Toluene (2)				Butoxyethanol (1) + <i>o</i> -Xylene (2)				Butoxyethanol (1) + <i>m</i> -Xylene (2)			
298.15	-0.069	-1.031	0.854	0.001	0.388	-2.116	1.487	0.001	0.102	1.487	0.667	0.001
303.15	0.032	-1.077	0.840	0.001	0.678	-2.096	1.026	0.001	0.387	-1.719	0.691	0.001
308.15	0.412	-1.161	0.091	0.001	0.789	-2.124	1.219	0.001	0.506	-1.993	1.047	0.001
313.15	0.558	-1.155	0.348	0.001	1.089	-2.202	1.210	0.001	0.862	-2.021	0.588	0.001
	Butoxyethanol (1) + <i>p</i> -Xylene (2)				Butoxyethanol (1) + Ethylbenzene (2)				Butoxyethanol (1) + Cyclohexane (2)			
298.15	-0.055	-1.333	0.635	0.001	0.183	-1.197	0.605	0.001	2.481	-1.553	0.191	0.001
303.15	0.064	-1.385	0.555	0.001	0.313	-1.261	0.868	0.001	2.436	-1.906	1.056	0.001
308.15	0.225	-1.431	0.586	0.001	0.599	-1.442	0.486	0.001	2.944	-1.232	0.306	0.001
313.15	0.746	-1.269	0.098	0.001	0.740	-1.626	0.447	0.001	3.067	-1.295	2.436	0.001

Table 4. Comparison of Excess Molar Volumes at Equimolar Composition (V_m^E) $_{x=0.5}$ with Literature Values for Alkoxyethanols + Aromatic Hydrocarbons and + Cyclohexane

	$(V_m^E)_{x=0.5}/\text{cm}^3 \cdot \text{mol}^{-1}$							
	$T = 298.15 \text{ K}$		$T = 303.15 \text{ K}$		$T = 308.15 \text{ K}$		$T = 313.15 \text{ K}$	
	present study	lit.	present study	lit.	present study	lit.	present study	lit.
methoxyethanol +								
benzene	0.137		0.174	0.174 ¹⁵	0.202		0.249	
toluene	0.152	0.1509 ⁴⁶	0.185	0.185 ¹⁵	0.211		0.270	
<i>o</i> -xylene	0.333		0.378		0.443		0.509	
<i>m</i> -xylene	0.275		0.313		0.356		0.423	
<i>p</i> -xylene	0.225		0.246		0.300		0.337	
ethylbenzene	0.252		0.281		0.332		0.383	
cyclohexane	0.894	0.9099 ¹⁹	0.950	0.9510 ¹⁹	1.015		1.053	
ethoxyethanol +								
benzene	0.126		-0.008	-0.0073 ¹⁴	-0.070		-0.136	-0.1356 ¹⁴
toluene	0.082	0.0823 ⁴⁶	0.110		0.135		0.151	
<i>o</i> -xylene	0.249		0.322		0.358		0.380	
<i>m</i> -xylene	0.149		0.242		0.293		0.353	
<i>p</i> -xylene	0.131		0.170		0.178		0.197	
ethylbenzene	0.171		0.216		0.237		0.274	
cyclohexane	0.793	0.795 ¹²	0.814	0.815 ¹²	0.847	0.844 ¹²	0.878	0.878 ¹²
butoxyethanol +								
benzene	0.076		0.093		0.132		0.153	
toluene	-0.017	-0.0056 ⁴⁶	0.008		0.103		0.140	
<i>o</i> -xylene	0.097		0.170		0.197		0.272	
<i>m</i> -xylene	0.026		0.097		0.127		0.216	
<i>p</i> -xylene	-0.014		0.016		0.056		0.187	
ethylbenzene	0.046		0.078		0.150		0.185	
cyclohexane	0.620		0.609		0.726		0.767	

$\pm 0.1 \text{ s}$, and the arithmetic mean was taken for the calculation of the viscosity. The estimated accuracy and

precision in viscosity measurements were found to be ± 0.002 and $\pm 0.001 \text{ mPa}\cdot\text{s}$, respectively. The speeds of

sound, v , were measured using an ultrasonic interferometer (Mittal Enterprises, New Delhi, India) operating at a fixed frequency of 2 MHz. The measured speeds of sound have a precision of $\pm 0.8 \text{ m}\cdot\text{s}^{-1}$ and an accuracy better than $\pm 1.9 \text{ m}\cdot\text{s}^{-1}$. The relative permittivities of the individual pure components and binary mixtures were calculated from the capacitance measurements with an universal dielectrometer, type OH-301 of Radelkis, Hungary. The procedure used in the calibration of dielectric cells was the same as that described in detail elsewhere.¹⁸ The measured relative permittivities have an estimated precision and accuracy of ± 0.001 and ± 0.004 , respectively. The desired temperatures accurate to $\pm 0.01 \text{ }^\circ\text{C}$ during the v and ϵ_r measurements were maintained using an INSREF, India, circulator (model 020A).

Results and Discussion

Densities, ρ , and Excess Molar Volumes, V_m^E . The experimental data on ρ at $T = (298.15, 303.15, 308.15, \text{ and } 313.15) \text{ K}$ for the 21 mixtures of methoxyethanol, ethoxyethanol, and butoxyethanol + benzene, + toluene, + *o*-xylene, + *m*-xylene, + *p*-xylene, + ethylbenzene, and + cyclohexane are listed in Table 2. The V_m^E values were calculated using the relation

$$V_m^E/\text{cm}^3\cdot\text{mol}^{-1} = \frac{x_1M_1 + x_2M_2}{\rho_{12}} - \left\{ \frac{x_1M_1}{\rho_1} + \frac{x_2M_2}{\rho_2} \right\} \quad (1)$$

The compositional variation of V_m^E was mathematically represented through the equation of the type

$$A^E = x_1(1 - x_1) \sum_{i=0}^{i=n} a_i(2x_1 - 1)^i \quad (2)$$

where $A^E = V_m^E$ and a_i are the fitting coefficients and x_1 is the alkoxyethanol mole fraction. The values of a_i were estimated by a least-squares method using multiple regression analysis. The summary of a_i and σ , the standard deviations between experimental and fitted V_m^E values, is given in Table 3. The graphical variation of V_m^E as a function of mole fraction of the alkoxyethanols for the binary systems of methoxyethanol, ethoxyethanol, and butoxyethanol + aromatic hydrocarbons and + cyclohexane at $T = 298.15 \text{ K}$ is shown in Figure 1. The V_m^E profiles of alkoxyethanols + aromatic hydrocarbons are characterized by initial positive values followed by small but negative values in the alkoxyethanol rich compositions. The binary mixtures containing cyclohexane as one of the components have, however, been characterized by large and positive values across the mole composition. The comparison of V_m^E values of the mixtures containing different alkoxyethanols + aromatic hydrocarbons and + cyclohexane showed that the positive magnitudes decreased on one hand and while the negative magnitudes increased on the other from methoxyethanol to butoxyethanol containing mixtures. The rise in the temperature from 298.15 to 313.15 K has always increased the overall magnitude of V_m^E values with an exception in ethoxyethanol + benzene mixtures. A comparison of our calculated equimolar V_m^E values with the literature data is presented in Table 4, and we noticed a close agreement of our data with the literature values.

The recent detailed ab initio calculations and a few matrix isolation infrared spectroscopy measurements have revealed that alkoxyethanol molecules in their pure monomeric (gas phase) state prefer the formation of five membered rings through $\text{CH}\cdots\text{O}$ and/or $\text{O}\cdots\text{H}-\text{O}$ con-

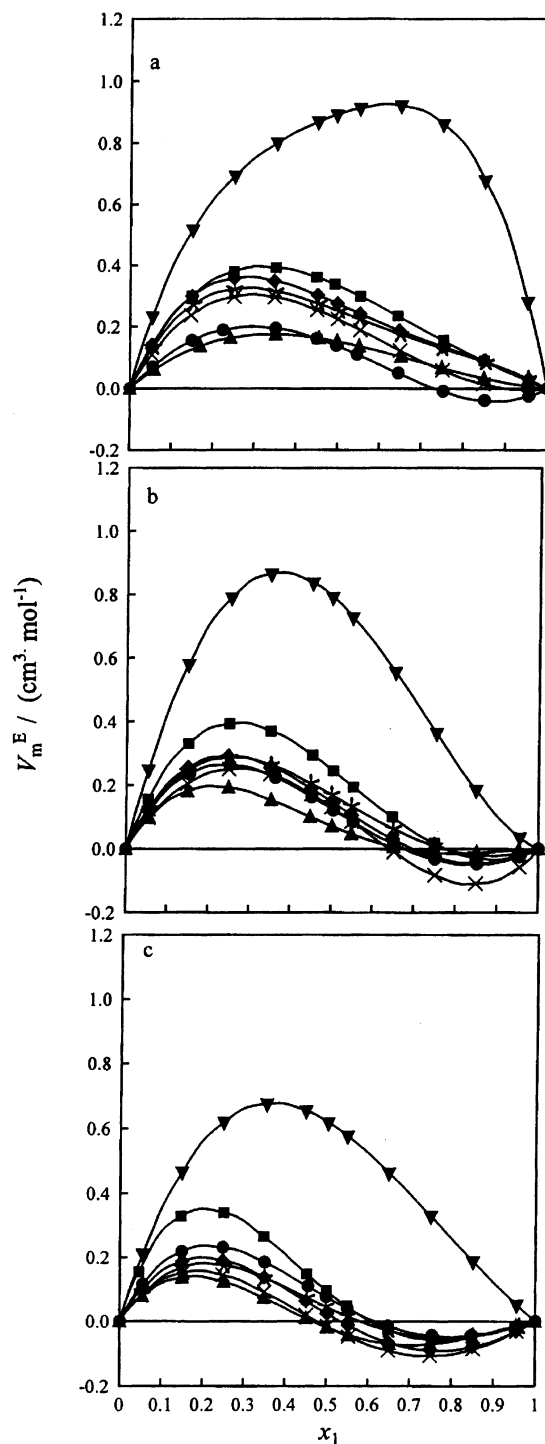


Figure 1. Variation of excess molar volumes, V_m^E , with alkoxyethanol mole fraction for the binary mixtures of methoxyethanol (a), ethoxyethanol (b), and butoxyethanol (c) + aromatic hydrocarbons and + cyclohexane at 298.15 K: ●, benzene; ▲, toluene; ■, *o*-xylene; ◆, *m*-xylene; ×, *p*-xylene; *, ethylbenzene; ▼, cyclohexane. Solid lines are fitted values calculated using coefficients from Table 3 and eq 2.

tacts between the methylene hydrogen and etheric oxygens or/and between the etheric oxygen and the hydrogen of the hydroxyl group of the same molecule.^{8-11,19} The binary systems of 1-alcohols + cyclohexane²⁰ exhibited large and positive volume expansions, and it has been reported that the heteroassociated structures of 1-alcohols were ruptured in the presence of cyclohexane. The molecular skeletons of methoxy-, ethoxy-, and butoxyethanols can be made structurally equivalent to 1-butanol, 1-pentanol, and 1-heptanol

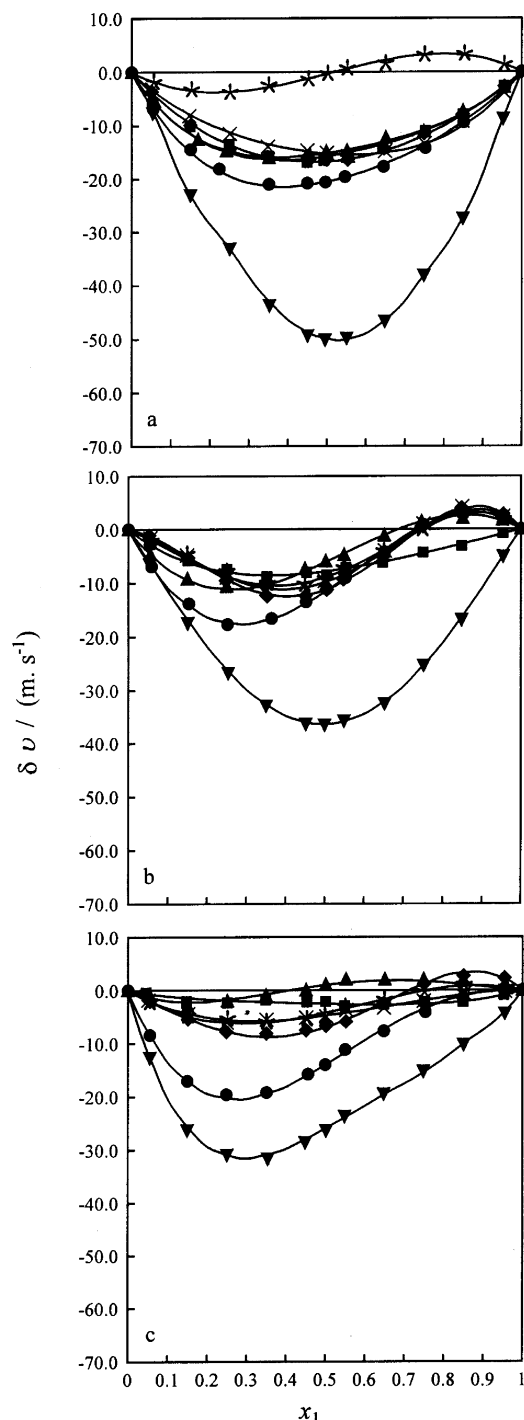


Figure 2. Variation of deviation in speeds of sound, δv , with alkoxyethanol mole fraction for the binary mixtures of methoxyethanol (a), ethoxyethanol (b), and butoxyethanol (c) + aromatic hydrocarbons and + cyclohexane at 298.15 K. (The symbols are the same as those in Figure 1.) Solid lines are fitted values calculated using coefficients from Table 6 and eq 2.

(the difference being the presence of an $-O-$ group in the place of $-CH_2-$). Our equimolar V_m^E values of 0.950, 0.814, and 0.609 for cyclohexane + methoxy-, + ethoxy-, and + butoxyethanols at $T = 303.15$ K are interestingly found to be smaller than 1.5355, 1.4668, and 1.3912 for cyclohexane + 1-butanol, + pentanol, and + 1-heptanol mixtures at the same temperature.²¹ Thus, we attribute the observed positive V_m^E values of alkoxyethanols + cyclohexane mixtures to the disruptions in the self-associated structures of the former. The smaller V_m^E values for

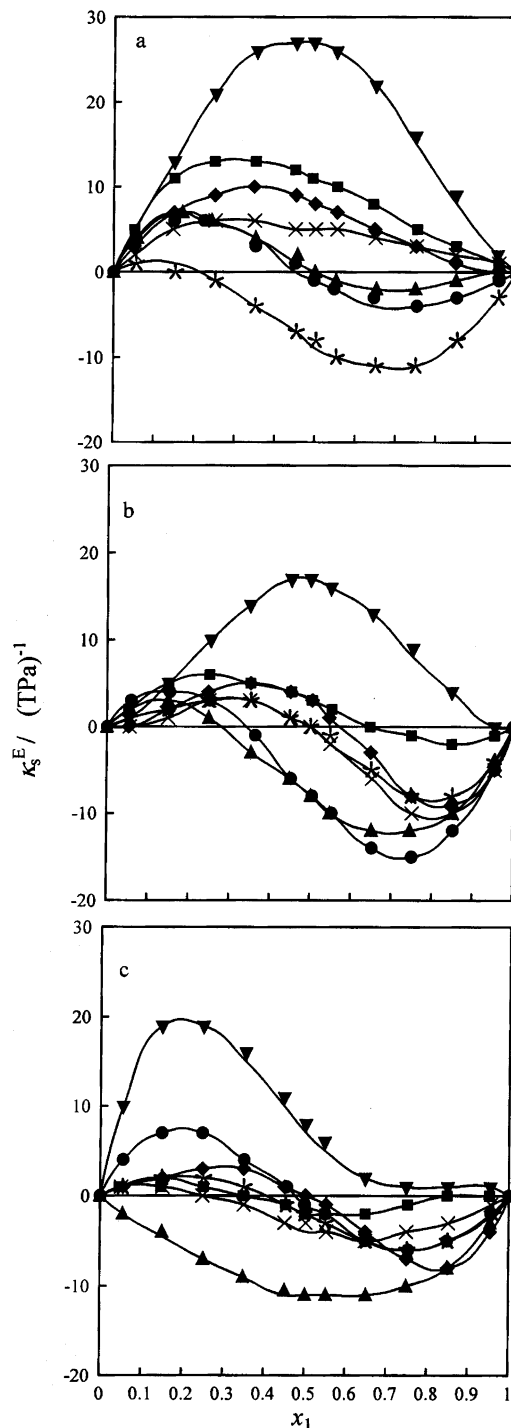


Figure 3. Variation of excess isentropic compressibilities, κ_s^E , with alkoxyethanol mole fraction for the binary mixtures of methoxyethanol (a), ethoxyethanol (b), and butoxyethanol (c) + aromatic hydrocarbons and + cyclohexane at 298.15 K. (The symbols are the same as those in Figure 1.) Solid lines are fitted values calculated using coefficients from Table 6 and eq 2.

alkoxyethanols + cyclohexane vis-à-vis those of 1-alcohols + cyclohexane indicate that the self-associate ring structures in the alkoxyethanols resist the structure disruption. The observed less positive or even negative V_m^E values for the alkoxyethanols + aromatic hydrocarbons in general indicate that, besides structure disruptions, weak interactions between the π electrons of the aromatic ring system and the etheric oxygen as well as the $-OH$ group of the respective alkoxyethanols also exist. The presence of one

Table 5. (Continued)

x_1	$\eta/\text{mPa}\cdot\text{s}$		$\nu/\text{m}\cdot\text{s}^{-1}$		ϵ_r		x_1	$\eta/\text{mPa}\cdot\text{s}$		$\nu/\text{m}\cdot\text{s}^{-1}$		ϵ_r	
	298.15 K	308.15 K	298.15 K	308.15 K	298.15 K	308.15 K		298.15 K	308.15 K	298.15 K	308.15 K	298.15 K	308.15 K
2-Ethoxyethanol (1) + Ethylbenzene (2)							2-Ethoxyethanol (1) + Cyclohexane (2)						
0.0573	0.658	0.557	1315	1272	2.778	2.713	0.0542	0.903	0.755	1249	1204	2.341	2.251
0.1487	0.696	0.597	1311	1267	3.288	3.292	0.1507	0.920	0.775	1242	1195	3.016	2.943
0.2498	0.749	0.648	1306	1265	3.839	3.955	0.2541	0.952	0.805	1237	1191	3.829	3.758
0.3527	0.817	0.708	1302	1264	4.558	4.739	0.3508	0.996	0.841	1235	1193	4.695	4.596
0.4489	0.895	0.773	1300	1264	5.467	5.619	0.4520	1.057	0.888	1236	1198	5.725	5.557
0.4998	0.944	0.812	1300	1264	6.053	6.149	0.5000	1.093	0.915	1238	1202	6.258	6.046
0.5485	0.995	0.852	1301	1264	6.682	6.695	0.5497	1.135	0.945	1241	1206	6.840	6.572
0.6501	1.121	0.945	1302	1264	8.174	7.944	0.6534	1.240	1.019	1249	1217	8.155	7.742
0.7484	1.273	1.050	1304	1264	9.763	9.242	0.7527	1.368	1.105	1260	1229	9.517	8.945
0.8508	1.469	1.178	1305	1264	11.399	10.591	0.8492	1.524	1.206	1274	1242	10.925	10.193
0.9547	1.721	1.331	1301	1265	12.784	11.822	0.9552	1.741	1.341	1294	1259	12.532	11.638
2-Butoxyethanol (1) + Benzene (2)							2-Butoxyethanol (1) + Toluene (2)						
0.0553	0.648	0.562	1291	1255	2.887	2.764	0.0550	0.593	0.531	1303	1261	2.977	2.817
0.1496	0.736	0.631	1283	1250	3.844	3.575	0.1509	0.678	0.597	1301	1260	3.879	3.536
0.2488	0.845	0.717	1281	1249	4.746	4.350	0.2513	0.784	0.679	1302	1261	4.730	4.242
0.3504	0.978	0.821	1282	1250	5.579	5.074	0.3489	0.909	0.775	1303	1262	5.497	4.887
0.4555	1.144	0.949	1286	1254	6.360	5.757	0.4511	1.066	0.896	1304	1264	6.256	5.527
0.4995	1.223	1.011	1288	1256	6.666	6.025	0.5015	1.156	0.965	1305	1265	6.618	5.830
0.5504	1.323	1.088	1291	1258	7.006	6.323	0.5525	1.257	1.042	1306	1267	6.974	6.128
0.6482	1.543	1.258	1295	1262	7.622	6.857	0.6512	1.483	1.215	1306	1270	7.639	6.682
0.7535	1.830	1.479	1299	1268	8.231	7.378	0.7494	1.759	1.425	1306	1273	8.255	7.200
0.8483	2.143	1.718	1302	1273	8.735	7.795	0.8498	2.105	1.689	1306	1277	8.815	7.695
0.9556	2.575	2.048	1304	1281	9.251	8.205	0.9541	2.551	2.030	1305	1282	9.287	8.763
2-Butoxyethanol (1) + <i>o</i> -Xylene (2)							2-Butoxyethanol (1) + <i>m</i> -Xylene (2)						
0.0549	0.797	0.686	1345	1314	2.838	2.852	0.0560	0.625	0.534	1317	1279	2.670	2.618
0.1475	0.891	0.756	1339	1303	3.513	3.387	0.1520	0.711	0.602	1312	1275	3.248	3.181
0.2508	1.004	0.840	1334	1295	4.248	3.995	0.2496	0.813	0.686	1308	1272	3.875	3.776
0.3485	1.129	0.933	1330	1291	4.975	4.572	0.3506	0.941	0.786	1306	1270	4.553	4.400
0.4527	1.286	1.052	1325	1288	5.769	5.186	0.4512	1.095	0.908	1305	1270	5.248	5.014
0.5000	1.366	1.113	1323	1287	6.131	5.463	0.5022	1.185	0.979	1305	1270	5.606	5.320
0.5489	1.457	1.182	1320	1286	6.504	5.749	0.5529	1.284	1.056	1305	1270	5.965	5.622
0.6483	1.666	1.341	1316	1278	7.248	6.327	0.6487	1.501	1.225	1307	1271	6.653	6.186
0.7518	1.925	1.540	1312	1282	7.985	6.924	0.7505	1.781	1.442	1309	1273	7.407	6.782
0.8493	2.216	1.765	1308	1281	8.622	7.484	0.8511	2.122	1.704	1309	1277	8.186	7.385
0.9524	2.586	2.053	1305	1283	9.211	8.077	0.9549	2.560	2.037	1307	1282	9.048	8.046
2-Butoxyethanol (1) + <i>p</i> -Xylene (2)							2-Butoxyethanol (1) + Ethylbenzene (2)						
0.0541	0.647	0.566	1306	1273	2.588	2.515	0.0546	0.678	0.568	1315	1274	2.659	2.616
0.1518	0.725	0.625	1303	1268	3.246	3.207	0.1505	0.769	0.643	1311	1272	3.289	3.166
0.2496	0.817	0.695	1301	1266	3.922	3.868	0.2513	0.877	0.732	1309	1270	3.977	3.780
0.3502	0.933	0.784	1301	1265	4.661	4.525	0.3501	1.003	0.835	1307	1270	4.671	4.391
0.4510	1.076	0.894	1301	1265	5.439	5.165	0.4528	1.161	0.961	1306	1271	5.391	5.020
0.5028	1.162	0.961	1301	1266	5.850	5.489	0.4982	1.240	1.025	1306	1271	5.706	5.293
0.5533	1.256	1.033	1302	1266	6.256	5.801	0.5500	1.339	1.103	1307	1272	6.064	5.602
0.6489	1.465	1.194	1302	1268	7.025	6.380	0.6497	1.560	1.277	1307	1274	6.747	6.190
0.7493	1.739	1.404	1303	1272	7.813	6.975	0.7511	1.831	1.487	1307	1276	7.454	6.783
0.8519	2.092	1.676	1304	1276	8.561	7.561	0.8507	2.156	1.736	1307	1279	8.186	7.379
0.9561	2.551	2.029	1304	1282	9.215	8.125	0.9614	2.601	2.071	1305	1283	9.095	8.087
2-Butoxyethanol (1) + Cyclohexane (2)													
0.0557	0.950	0.790	1244	1206	2.372	2.238							
0.1501	1.046	0.866	1236	1202	3.018	2.869							
0.2504	1.162	0.958	1237	1202	3.704	3.556							
0.3543	1.300	1.066	1242	1206	4.419	4.260							
0.4488	1.443	1.178	1250	1212	5.080	4.885							
0.5025	1.532	1.248	1255	1216	5.461	5.228							
0.5493	1.616	1.313	1260	1220	5.799	5.521							
0.6485	1.813	1.465	1269	1229	6.534	6.127							
0.7494	2.043	1.642	1278	1241	7.313	6.733							
0.8511	2.311	1.848	1287	1255	8.140	7.354							
0.9556	2.631	2.091	1298	1275	9.043	8.037							

or two $-\text{CH}_3$ groups and the CH_3-CH_2- group on the aromatic ring system affects the balance between the above-mentioned opposing effects due to steric hindrance.

Dynamic Viscosities, η . The experimentally measured η values for the 21 mixtures at $T = (298.15 \text{ and } 308.15) \text{ K}$ are listed in Table 5. The one parameter Grunberg–Nissan

Table 6. Parameters of Eq 2 for the Mathematical Representation of Various Excess and Deviation Functions for Alkoxyethanols (1) + Aromatic Hydrocarbons (2) and + Cyclohexane (2) at $T = (298.15$ and $308.15)$ K

	$T = 298.15$ K				$T = 308.15$ K				$T = 298.15$ K				$T = 308.15$ K			
	a_0	a_1	a_2	σ	a_0	a_1	a_2	σ	a_0	a_1	a_2	σ	a_0	a_1	a_2	σ
	Methoxyethanol (1) + Benzene (2)								Methoxyethanol (1) + Toluene (2)							
$\delta v/m \cdot s^{-1}$	-81.9	31.0	-25.3	0.4	-104.3	-12.1	-14.6	0.5	-60.3	21.1	-30.2	0.4	-91.1	-41.4	-28.0	0.3
κ_s^E/TPa^{-1}	-5	-39	47	1.0	12	1	11	0.1	0.4	-34	35	0.5	31	18	14	0.9
$\delta \epsilon_r$	-6.962	5.652	6.966	0.001	-4.106	4.429	4.017	0.001	-4.995	5.248	7.054	0.001	-3.254	4.486	3.329	0.001
	Methoxyethanol (1) + <i>o</i> -Xylene (2)								Methoxyethanol (1) + <i>m</i> -Xylene (2)							
$\delta v/m \cdot s^{-1}$	-62.9	21.9	-25.8	0.4	-118.0	-0.0	-65.6	0.4	-66.7	8.9	-3.7	0.4	-94.3	-5.9	-24.3	0.3
κ_s^E/TPa^{-1}	45	-36	18	1.0	106	-18	55	0.6	31	-28	14	0.8	61	-19	7	0.5
$\delta \epsilon_r$	-3.700	0.947	0.980	0.001	-3.623	0.227	0.192	0.001	-3.375	3.342	3.975	0.002	-3.052	6.600	7.289	0.001
	Methoxyethanol (1) + <i>p</i> -Xylene (2)								Methoxyethanol (1) + Ethylbenzene (2)							
$\delta v/m \cdot s^{-1}$	-60.9	-11.5	-18.6	0.4	-99.1	-44.3	-45.4	0.4	-1.4	36.6	1.2	0.3	-96.3	-40.9	-46.5	0.4
κ_s^E/TPa^{-1}	18	-14	13	0.7	60	9	29	0.7	35	-50	14	0.5	60	2	39	0.6
$\delta \epsilon_r$	-4.017	3.307	4.979	0.001	-2.438	4.640	3.778	0.001	-4.950	3.396	5.767	0.001	-3.022	4.469	3.636	0.002
	Methoxyethanol (1) + Cyclohexane (2)								Ethoxyethanol (1) + Benzene (2)							
$\delta v/m \cdot s^{-1}$	-199.6	-26.1	41.1	0.3	-230.7	79.0	99.3	0.4	-46.4	94.8	7.2	0.3	-51.7	12.7	25.4	0.3
κ_s^E/TPa^{-1}	108	-22	-59	1.6	146	-7	87	1.3	-32	-94	2	0.1	-28	5	-28	0.1
$\delta \epsilon_r$	-6.845	1.251	2.129	0.001	-4.041	0.756	-1.257	0.001	-5.007	3.866	4.577	0.001	-2.547	4.830	0.701	0.001
	Ethoxyethanol (1) + Toluene (2)								Ethoxyethanol (1) + <i>o</i> -Xylene (2)							
$\delta v/m \cdot s^{-1}$	-24.6	66.9	-3.1	0.3	-27.8	32.3	-23.7	0.3	-31.5	18.4	-6.4	0.4	-74.6	32.0	17.4	0.4
κ_s^E/TPa^{-1}	-33	-71	10	0.1	-25	-44	28	0.4	13	-35	-2	0.5	62	-41	-25	0.1
$\delta \epsilon_r$	-2.268	2.906	3.216	0.001	-0.769	2.393	2.073	0.001	-2.437	3.348	3.139	0.001	-2.817	2.236	2.971	0.001
	Ethoxyethanol (1) + <i>m</i> -Xylene (2)								Ethoxyethanol (1) + <i>p</i> -Xylene (2)							
$\delta v/m \cdot s^{-1}$	-44.8	50.0	81.4	0.3	-41.6	53.7	31.2	0.3	-39.4	47.4	65.6	0.5	-55.3	55.9	-12.4	0.2
κ_s^E/TPa^{-1}	12	-63	-85	0.1	15	-60	-38	0.5	-1	64	-70	0.1	25	-68	15	0.4
$\delta \epsilon_r$	-2.121	3.739	3.879	0.001	-1.603	2.592	1.705	0.001	-3.375	3.581	4.461	0.001	-1.740	1.341	3.882	0.001
	Ethoxyethanol (1) + Ethylbenzene (2)								Ethoxyethanol (1) + Cyclohexane (2)							
$\delta v/m \cdot s^{-1}$	-35.7	46.3	50.2	0.4	-30.7	19.1	-26.7	0.2	-145.4	2.7	32.9	0.4	-144.0	56.7	-14.9	0.4
κ_s^E/TPa^{-1}	0	-59	-46	0.4	2	-31	34	0.5	67	-7	-70	0.4	66	-97	29	0.4
$\delta \epsilon_r$	-4.438	3.105	6.953	0.001	-2.234	2.058	3.722	0.001	-4.147	0.441	0.908	0.001	-2.945	0.048	0.345	0.001
	Butoxyethanol (1) + Benzene (2)								Butoxyethanol (1) + Toluene (2)							
$\delta v/m \cdot s^{-1}$	-56.0	89.0	-29.9	0.4	-76.9	33.7	-35.4	0.3	4.1	18.4	-17.1	0.4	-37.3	2.7	-15.3	0.4
κ_s^E/TPa^{-1}	-3	-69	22	0.4	20	0	29	0.4	-42	-26	-1	0.1	16	0	-19	0.1
$\delta \epsilon_r$	0.489	-0.177	0.288	0.001	0.590	0.187	0.214	0.001	1.245	0.268	1.098	0.001	0.459	0.088	0.203	0.001
	Butoxyethanol (1) + <i>o</i> -Xylene (2)								Butoxyethanol (1) + <i>m</i> -Xylene (2)							
$\delta v/m \cdot s^{-1}$	-9.9	-3.5	-7.6	0.4	-63.0	27.4	-52.2	0.2	-27.7	47.6	41.3	0.4	-56.5	3.9	-18.0	
κ_s^E/TPa^{-1}	-6	-10	22	0.4	56	-36	57	0.5	1	-56	-46	0.4	40	-8	14	0.1
$\delta \epsilon_r$	-0.052	1.525	0.208	0.001	-0.395	0.086	-0.121	0.001	-1.719	-0.080	-0.593	0.001	-0.484	-0.091	-0.724	0.001
	Butoxyethanol (1) + <i>p</i> -Xylene (2)								Butoxyethanol (1) + Ethylbenzene (2)							
$\delta v/m \cdot s^{-1}$	-19.0	19.3	-2.6	0.3	-60.7	6.8	-9.0	0.4	-16.9	31.6	1.8	0.4	-36.8	4.6	-12.6	0.4
κ_s^E/TPa^{-1}	-14	-24	14	0.4	39	0	32	0.5	-8	-41	-9	0.1	15	-10	22	0.4
$\delta \epsilon_r$	-0.561	1.631	0.776	0.001	0.570	-0.028	0.262	0.001	-1.251	-0.287	-1.264	0.001	-0.530	-0.054	-0.803	0.001
	Butoxyethanol (1) + Cyclohexane (2)															
$\delta v/m \cdot s^{-1}$	-103.7	82.6	-78.8	0.4	-144.5	15.8	-54.6	0.3								
κ_s^E/TPa^{-1}	30	-98	98	0.4	81	-32	82	0.4								
$\delta \epsilon_r$	-2.530	-0.458	-0.060	0.001	-0.842	-0.145	-0.961	0.001								

(GN), two parameter McAllister (Mc), and three parameter Auslander (A) equations were employed to correlate the dynamic and kinematic viscosities, η , ν , and viscosity ratios.

$$\ln \eta_{12} = x_1 \ln \eta_1 + x_2 \ln \eta_2 + x_1 x_2 G_{12} \quad (3)$$

$$\ln \nu_{12} = x_1^3 \ln \nu_1 + 3x_1^2 x_2 \ln M_{12} + 3x_1 x_2^2 \ln M_{21} + x_2^3 \ln \nu_2 - \ln \left(x_1 + \frac{x_2 M_2}{M_1} \right) + 3x_1^2 x_2 \ln \left(\frac{2}{3} + \frac{M_2}{3M_1} \right) + 3x_1 x_2^2 \ln \left(\frac{1}{3} + \frac{2M_2}{3M_1} \right) + x_2^3 \ln \left(\frac{M_2}{M_1} \right) \quad (4)$$

$$x_1(x_1 + B_{12}x_2)(\eta_{12} - \eta_1) + A_{21}x_2(B_{21}x_1 + x_2)(\eta_{12} - \eta_2) = 0 \quad (5)$$

These equations are particularly selected because the characteristic constant parameter G_{12} of eq 3 allows for the positive and negative deviations from the additivity rule,

eq 4 is based on Eyring theory on absolute reaction rates with a three body model, and eq 5 involves three parameters. The Grunberg–Nissan and McAllister equations correlated the viscosities excellently with maximum σ values of 0.001 mPa·s. However, the application of the Auslander equation has yielded σ values ranging from 0.013 to 0.146.

Speeds of Sound, v , and Excess Isentropic Compressibilities, κ_s^E . The data of experimental speeds of sound are listed in Table 5. The speeds of sound were also calculated using free length theory (FLT) and collision factor theory (CFT) approaches and Nomoto and Junjie equations.²² The various thermophysical quantities of pure liquids needed for the calculation of speeds of sound have been listed in Table 1. The standard percentage deviation, $\sigma\%$, for the experimental and predicted values ranged from 0.4 to 13.4 for different approaches. Hence, it is stated that the above four approaches fail to predict the speeds of sound in these mixtures.

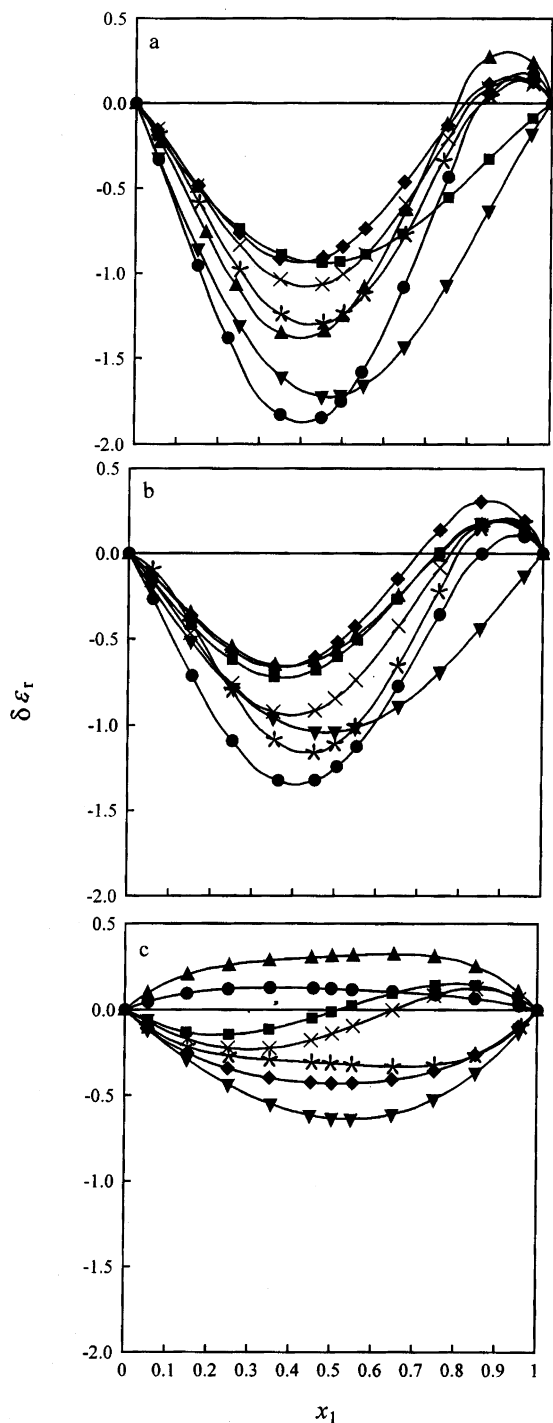


Figure 4. Variation of relative permittivity deviations, $\delta\epsilon_r$, with alkoxyethanol mole fraction for the binary mixtures of methoxyethanol (a), ethoxyethanol (b), and butoxyethanol (c) + aromatic hydrocarbons and + cyclohexane at 298.15 K. (The symbols are the same as those in Figure 1.) Solid lines are fitted values calculated using coefficients from Table 6 and eq 2.

The deviations in speed of sound, δv , and excess isentropic compressibilities, κ_s^E , were calculated using the relations

$$\delta v/\text{m}\cdot\text{s}^{-1} = v_{12} - (\phi_1 v_1 + \phi_2 v_2) \quad (6)$$

$$\kappa_s^E/\text{TPa}^{-1} = \kappa_s - \kappa_s^{\text{id}} \quad (7)$$

where κ_s is the isentropic compressibility and was calcu-

lated using the Laplace equation, that is, $\kappa_s = 1/(v^2\rho)$, and κ_s^{id} was calculated from the relation

$$\kappa_s^{\text{id}} = \sum_{i=1}^2 \phi_i [\kappa_{s,i} + TV_i(\alpha_i^2)/C_{p,i}] - \{T(\sum_{i=1}^2 x_i V_i) (\sum_{i=1}^2 \phi_i \alpha_i)^2 / \sum_{i=1}^2 x_i C_{p,i}\} \quad (8)$$

and the ϕ_i is the ideal state volume fraction and is defined by the relation

$$\phi_i = x_i V_i / (\sum_{i=1}^2 x_i V_i) \quad (9)$$

The δv and κ_s^E are also smoothed through use of eq 2. The summary of the smoothing coefficients, a_b , and σ values is given in Table 6. The maximum uncertainties in δv and κ_s^E values have been found to be $0.5 \text{ m}\cdot\text{s}^{-1}$ and 0.9 TPa^{-1} . The variation of δv as a function of alkoxyethanol mole fraction for the binary mixtures at $T = 298.15 \text{ K}$ is shown in Figure 2. It can be seen from the figure that, for methoxyethanol containing mixtures, the δv values in general are large and negative except for the case of methoxyethanol + ethylbenzene, in which the profile showed an initial negative trend followed by positive points. Except in benzene containing mixtures, the δv values at equimole composition (i.e. $x_1 = 0.5$) have been found to be shifted to lesser negative magnitudes from methoxyethanol to ethoxyethanol to butoxyethanol. The rise in the temperature in general, however, tends to increase the negative δv values. The graphical variation of κ_s^E as a function of alkoxyethanol mole fraction for the binary mixtures at $T = 298.15 \text{ K}$ is shown in Figure 3. The κ_s^E values in cyclohexane containing mixtures at $T = 298.15 \text{ K}$ have been found to be large and positive in methoxyethanol and ethoxyethanol containing mixtures. The κ_s^E values, however, become less positive in the 2-butoxyethanol rich regions. The positive κ_s^E values indicate that the mixed species are overall more compressible and hence have large volumes due to the structure disruption effect of cyclohexane. The κ_s^E values in methoxyethanol + benzene, + toluene, + ethylbenzene and in ethoxyethanol and butoxyethanol + six aromatics have been found to be negative, especially in the alkoxyethanol rich region and at $T = 298.15 \text{ K}$. The rise in the temperature from $T = (298.15 \text{ to } 308.15) \text{ K}$ increased the magnitude of κ_s^E values in these mixtures. The negative κ_s^E values indicate the dominance of weak but structure making $\text{n}\cdot\cdot\pi$, $-\text{OH}\cdot\cdot\pi$, and $-\text{CH}\cdot\cdot\pi$ interactions at $T = 298.15 \text{ K}$, and the same get further weakened at elevated temperatures due to enhanced thermal motion.

Deviations in Relative Permittivities, $\delta\epsilon_r$. The $\delta\epsilon_r$ values are calculated using $\epsilon_{r,1}$ and $\epsilon_{r,12}$ values as listed in Tables 1 and 5 through the relation

$$\delta\epsilon_r = \epsilon_{r,12} - (\phi_1 \epsilon_{r,1} + \phi_2 \epsilon_{r,2}) \quad (10)$$

The values of the coefficients a_i needed for the mathematical representation of $\delta\epsilon_r$ and σ between the experimental and fitted values are listed in Table 6. The graphical representations of $\delta\epsilon_r$ as a function of alkoxyethanol mole fractions for the binary mixtures at $T = 298.15 \text{ K}$ are shown in Figure 4. The profiles showed that $\delta\epsilon_r$ values in methoxyethanol containing mixtures are largely negative except a few small but positive points to the right of the figure.

The magnitude of $\delta\epsilon_i$ values, however, was found to become less negative with the lengthening of alkyl chain in ethoxyethanol and butoxyethanol and also with the rise in the temperature. We did not, however, find any definite trend in $(\delta\epsilon_i)_{0.5}$ values among different aromatics for a given alkoxyethanol.

Acknowledgment

The authors thank Prof. Dr. R. M. Patel, the head of the department, for providing necessary laboratory facilities.

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Received for review January 7, 2003. Accepted April 23, 2003.

JE034005Y